

**BEFORE THE ILLINOIS POLLUTION CONTROL BOARD**

SEP 12 2005

IN THE MATTER OF: )  
)  
PETITION OF LAFARGE MIDWEST, INC. )  
FOR AN ADJUSTED STANDARD )  
FROM 35 Ill. Adm. Code 739.161 )  
PURSUANT TO 35 Ill. Adm. Code 720.132 and )  
720.133. )

AS dc - 001 STATE OF ILLINOIS  
Pollution Control Board

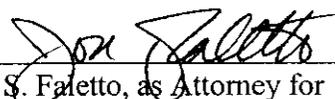
**NOTICE OF FILING**

TO: Illinois Pollution Control Board  
Attn: Dorothy M. Gunn, Clerk  
100 West Randolph Street  
James R. Thompson Center, Suite 11-500  
Chicago, IL 60601-3218

Division of Legal Counsel  
Illinois Environmental Protection Agency  
1021 North Grand Avenue East  
P.O. Box 19276  
Springfield, IL 62794-9276

PLEASE TAKE NOTICE that on this 7<sup>th</sup> day of September, 2005, a copy of the attached *Petition for Adjusted Standard* was filed with the Office of the Clerk of the Illinois Pollution Control Board, a copy of which is herewith served on you.

Respectfully submitted,

  
\_\_\_\_\_  
Jon S. Faletto, as Attorney for  
Petitioner Lafarge Midwest, Inc.

Jon S. Faletto  
Howard & Howard Attorneys, P.C.  
One Technology Plaza, Suite 600  
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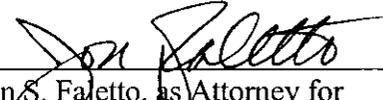
**CERTIFICATE OF SERVICE**

I, the undersigned, certify that I have served the attached *Petition for Adjusted Standard* upon the person or agency to whom it is directed, by placing it in an envelope addressed to:

Illinois Pollution Control Board  
Attn: Dorothy M. Gunn, Clerk  
100 West Randolph Street  
James R. Thompson Center, Suite 11-500  
Chicago, IL 60601-3218

Division of Legal Counsel  
Illinois Environmental Protection Agency  
1021 North Grand Avenue East  
P.O. Box 19276  
Springfield, IL 62794-9276

and mailing it via First Class U.S. Mail from Peoria, Illinois, on this 7<sup>th</sup> day of September, 2005, with sufficient postage affixed thereto.

  
\_\_\_\_\_  
Jon S. Faletto, as Attorney for  
Petitioner Lafarge Midwest, Inc.

Jon S. Faletto  
Howard & Howard Attorneys, P.C.  
One Technology Plaza, Suite 600  
211 Fulton Street  
Peoria, IL 61602  
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SEP 17 2005

BEFORE THE ILLINOIS POLLUTION CONTROL BOARD STATE OF ILLINOIS  
Pollution Control Board

IN THE MATTER OF: )  
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PETITION OF LAFARGE MIDWEST, INC. ) AS de. 021  
FOR AN ADJUSTED STANDARD )  
FROM 35 Ill. Adm. Code 739.161 )  
PURSUANT TO 35 Ill. Adm. Code 720.132 and )  
720.133. )

**PETITION FOR ADJUSTED STANDARD**

NOW COMES the Petitioner, LAFARGE MIDWEST, INC., by and through its attorneys, Howard & Howard Attorneys, P. C., and presents to the Illinois Pollution Control Board ("Board") its Petition for Adjusted Standard pursuant to 35 Ill. Adm. Code 720.133 requesting a determination that certain equipment be considered an "industrial boiler" as that term is defined in 35 Ill. Adm. Code 720.110. The Board regulations at 35 Ill. Adm. Code 720.132 provide that the Board will make such a determination on a case-by-case basis utilizing the Adjusted Standard procedures of Subpart D of 35 Ill. Adm. Code 104.

In support of its Petition, the Petitioner states as follows:

**I. Description of Petitioner and South Chicago Facility**

The South Chicago Slag Grinding Plant ("Grinding Plant") is owned and operated by Lafarge Midwest, Inc. ("Lafarge"), a subsidiary of Lafarge North America, Inc. Together with its subsidiaries, Lafarge North America is the largest supplier of cement and a leading ready-mixed concrete supplier in North America. The Company also is one of the top four producers of construction aggregate (crushed stone, sand and gravel) and a leading manufacturer of gypsum drywall. Lafarge North America has over 1,000 operations doing business in almost every State and throughout all provinces in Canada through its Lafarge Canada, Inc. subsidiary. Lafarge's products are used in the construction of such diverse projects as roads, office buildings, factories,

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hospitals, department stores, sports stadiums, banks, museums, high-rise apartments, amusement parks, swimming pools and bridges. In 2002, Lafarge North America shipped 117.1 million tons of aggregate, 11.1 million cubic yards of ready-mixed concrete, 13.8 million tons of cement and 2.0 billion square feet of gypsum drywall.

Lafarge developed the South Chicago Slag Grinding Plant in 2001 and 2002. The plant was developed on existing Lafarge property that had been used as a terminal for cement product storage and distribution since approximately 1987. The Grinding Plant is located at the common address of 2150 East 130<sup>th</sup> Street, Cook County, Chicago, Illinois, adjacent to the Calumet River and the southernmost portion of Lake Calumet.

The Lake Calumet area is a heavily industrialized area of active and closed steel mills, oil refineries, railroad yards, coke ovens, heavy manufacturing and waste disposal facilities. Waste disposal facilities are a major land feature of the landscape; five major facilities – Paxton I, Paxton II, Land & Lakes, CID No.1, and CID No. 2 – cover approximately 820 acres in the Lake Calumet area, with only Waste Management’s CID No.2 landfill currently operating. An aerial photograph showing the Grinding Plant is attached as Exhibit A. In addition, a map showing the location of the Grinding Plant and low population density of the surrounding Lake Calumet area is attached hereto as Exhibit B.

The economy and communities in the Lake Calumet area are still recovering from the loss of several steel mills, including Wisconsin Steel (1980), U.S. Steel Company’s South Works (1992), LTV and Acme Steel (2003), and the closing of the many area businesses that supported the steel industry. The Lake Calumet area has vast acres of vacant land available for industrial development; at least 1,000 acres of vacant property is identified as available for industrial uses in the City of Chicago’s 2002 *Calumet Area Land Use Plan*. That Land Use Plan designates

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property in the Lake Calumet area for future industrial development and open space, but no property is designated for future residential development.

Sustainable development, using a byproduct from another industry, was one of the key factors in Lafarge's decision to construct the Grinding Plant at this location. The principal product produced by Lafarge's Grinding Plant is a slag cement product marketed under the trade name "NewCem®". NewCem is produced by drying and grinding a pelletized or granulated iron blast furnace slag to cement fineness. The blast furnace slag used by Lafarge in the production of NewCem is generated at the Ispat-Inland, Inc. integrated steel facility located in East Chicago, Indiana, approximately 20 miles away.

Blast furnaces, which produce iron from iron ore in the presence of limestone or dolomite fluxes produce a molten slag. The molten slag is tapped off the furnace separately from the iron and quenched with water through a granulation or pelletizing process. Modern blast furnaces produce slag having a very low variability. Typically, the oxide forms of silicon, calcium, aluminum and magnesium make up 95% or more of the blast furnace slag.

Slag cement such as Lafarge's NewCem product can be used to replace a portion of the cement in a concrete mix. The advantages of slag cement are improved workability and pumpability in the plastic (unhardened) form of concrete. In hardened concrete, the use of slag cement increases strength, reduces permeability and heat of hydration, increases sulfate resistance and controls the alkali/silica reaction.

The environmental benefits associated with production of NewCem slag cement include productive use of an industrial byproduct, i.e. blast furnace slag, that otherwise would be landfilled, reduced use of virgin materials and substantially reduced energy consumption compared to the energy demands of Portland cement manufacturing. Lafarge's proposal to

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utilize off-specification used oil fuel in the slag drying process provides additional environmental benefits by recycling and reclaiming the thermal energy from the waste oils that are generated from motor vehicles, refineries and manufacturing processes using machining/cutting oils, heat transfer fluids, hydraulic fluids and general lubricants.

The U. S. Environmental Protection Agency (“USEPA”) has actively promoted and approved the recycling of used oil for energy recovery since Congress passed the Used Oil Recycling Act in 1980. Consistent with the legislative mandate to adopt a hazardous and solid waste management program consistent with the federal program and to secure USEPA approval thereof, the Board has adopted “identical-in-substance” regulations designed to encourage used oil recycling and burning specification and off-specification used oil for energy recovery.

Utilization of off-specification used oil fuel in the slag drying system at the Lafarge Grinding Plant is not expected to change the current air emissions from the facility, other than a negligible increase in the emissions of sulfur dioxide emissions from the drying operation. The air emissions associated with the proposed use of off-specification used oil fuel will be subject to approval by the IEPA through modification of the Grinding Plant’s existing Lifetime Operating Permit. The permit modification procedures will provide the opportunity to address any questions related to emissions of air contaminants associated with the combustion of used oil fuels.

## **II. Petition Content Requirements of 35 Ill. Adm. Code 104.406**

Set forth below is the information specified by 35 Ill. Admin. Code 104.406 required to be included in a Petition for Adjusted Standard. The information is organized under headings corresponding to the informational requirements of each subsection of Section 104.406, in compliance with that Section.

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- a) **A statement describing the standard from which an adjusted standard is sought. This must include the Illinois Administrative Code citation to the regulation of general applicability imposing the standard as well as the effective date of that regulation;**

**Response:** The Board has promulgated administrative regulations applicable to the management of used oil set forth at 35 Ill. Adm. Code Part 739. Subpart G of the Part 739 Standards for the Management of Used Oil allow the burning of off-specification used oil for energy recovery. The burning of off-specification used oil is allowed in certain devices specified in 35 Ill. Adm. Code Section 739.161(a), including “industrial boilers.” That regulation of general applicability states:

**Section 739.161      Restriction on Burning**

- a) Off-specification used oil fuel may only be burned for energy recovery in the following devices:
- 1) Industrial furnaces identified in 35 Ill. Adm. Code §720.110;
  - 2) Boilers, as defined in 35 Ill. Adm. Code 720.110, that are identified as follows:
    - A) Industrial boilers located on the site of a facility engaged in a manufacturing process where substances are transformed into new products, including the component parts of products, by mechanical or chemical processes;
    - B) Utility boilers used to produce electric power, steam, heated or cooled air, or other gases or fluids for sale; or
    - C) Used oil-fired space heaters provided that the burner meets the provisions of Section 739.123; or
  - 3) Hazardous waste incinerators subject to regulation under Subpart O of 35 Ill. Adm. Code 724 or 725.

The Board has promulgated regulations at 35 Ill. Adm. Code 720.132 and 720.133 establishing criteria and procedures for making a determination that certain enclosed devices using controlled flame combustion are “boilers” that may be utilized for the burning of off-

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specification used oil, even though such devices do not otherwise meet the definition of “boiler” contained in 35 Ill. Adm. Code 720.110. Section 720.132 establishes the criteria to be considered by the Board and Section 720.133 mandates use of the Adjusted Standard procedures of Subpart D of 35 Ill. Adm. Code 104 to determine whether a particular enclosed flame combustion device is a “boiler” that may be used to burn off-specification used oil.

Petitioner seeks an adjusted standard from 35 Ill. Adm. Code §739.161(a) pursuant to the criteria established by Section 720.132 and utilizing the procedures established by 720.133. The regulation of general applicability, specifically 35 Ill. Admin. Code 739.161(a), was promulgated with an effective date of July 19, 2004 (28 Ill. Reg. 10706, effective July 19, 2004).

- b) **A statement that indicates whether the regulation of general applicability was promulgated to implement, in whole or in part, the requirements of the CWA (33 USC 1251 et seq.), Safe Drinking Water Act (42 USC 300(f) et seq.), Comprehensive Environmental Response, Compensation and Liability Act (42 USC 9601 et seq.), CAA (42 USC 7401 et seq.), or the State programs concerning RCRA, UIC, or NPDES [415 ILCS 5/28.1];**

**Response:** The regulation of general applicability, 35 Ill. Adm. Code 739.161(a), was promulgated to implement, in whole or in part, the requirements of the Illinois program for the management of solid and hazardous waste, the state analog to the federal regulatory program under the Solid Waste Disposal Act, as amended by the Resource Conservation and Recovery Act, 42 U.S.C. §6901, et seq. (hereafter “RCRA”).

- c) **The level of justification as well as other information or requirements necessary for an adjusted standard as specified by the regulation of general applicability or a statement that the regulation of general applicability does not specify a level of justification or other requirements [415 ILCS 5/28.1] (See Section 104.426);**

**Response:** Although the regulation of general applicability from which relief is sought [35 Ill. Adm. Code 739.161(a)], does not specify the information or requirements necessary for an adjusted standard, the Board’s regulations at 35 Ill. Adm. Code 720.132 and

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720.133 establish the criteria and procedures for securing adjusted standard relief from 35 Ill. Adm. Code 739.161(a). Section 720.132 establishes the criteria to be considered by the Board for making a determination that certain enclosed devices using controlled flame combustion are “boilers” that may be utilized for burning off-specification used oil for energy recovery, even though such devices do not otherwise meet the definition of a “boiler” contained in 35 Ill. Adm. Code §720.110. (Note: Sections 720.132 and 720.133 are virtually identical to the federal RCRA regulations at 40 CFR 260.32 and 260.33 which establish the criteria and variance procedures for “case-by-case” determinations that specific combustion devices can be considered “boilers.”)

The criteria and procedures for securing adjusted standard relief from 35 Ill. Adm. Code 739.161(a) are set forth in Sections 720.132 and 720.133 which are set forth below:

**Section 720.132      Boiler Determinations**

In accordance with the standards and criteria in Section 720.110 (definition of “boiler”), and the procedures in 720.133, the Board will determine on a case-by-case basis that certain enclosed devices using controlled flame combustion are boilers, even though they do not otherwise meet the definition of boiler contained in Section 720.110, after considering the following criteria:

- a) The extent to which the unit has provisions for recovering and exporting thermal energy in the form of Steam, heated fluids or heated gasses;
- b) The extent to which the combustion chamber and energy recovery equipment are of integral design;
- c) The efficiency of energy recovery, calculated in terms of the recovered energy compared with the thermal value of the fuel;
- d) The extent to which exported energy is utilized;
- e) The extent to which the device is in common and customary use as a “boiler” functioning primarily to produce steam, heated fluids or heated gases; and
- f) Other relevant factors.

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(Source: Amended at 27 Ill. Reg. §12713, effective July 17, 2003.)

**Section 720.133      Procedures for Determinations**

The Board will use the procedures of Subpart D of 35 Ill. Adm. Code 104 for determining whether a material is a solid waste or for determining whether a particular enclosed flame combustion device is a boiler.

(Source: Amended at 27 Ill. Reg. §12713, effective July 17, 2003.)

- d) **A description of the nature of the petitioner's activity that is the subject of the proposed adjusted standard. The description must include the location of, and area affected by, the petitioner's activity. This description must also include the number of persons employed by the petitioner's facility at issue, age of that facility, relevant pollution control equipment already in use, and the qualitative and quantitative description of the nature of emissions, discharges or releases currently generated by the petitioner's activity;**

**Response:** The principal product produced by Lafarge at the South Chicago Slag Grinding Plant is a slag cement product marketed under the trade name "NewCem®". NewCem is a ground granulated blast furnace slag produced by grinding a pelletized or granulated blast furnace slag to cement fineness. The blast furnace slag used by Lafarge in the production of NewCem is generated at the Ispat-Inland, Inc. integrated steel mill located in East Chicago, Indiana, approximately 20 miles away.

Pelletized slag is delivered to the Grinding Plant via truck. The 10-12% moisture content of the slag guarantees a dust-free transfer of slag from the truck to the raw material storage hoppers at the Grinding Plant. From the storage hoppers, raw material is moved via conveyors and elevators through the Grinding Plant where any metallic compounds are removed via magnets before the slag is introduced into the drying system. The slag dryer functions as a direct-fired process heater to reduce the moisture content of the blast furnace slag so that the slag can be ground into a fine powder and processed into slag cement. The dried slag discharges to a cyclone collector before being fed to a large ball mill to reduce the slag to a fine powder and

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achieve product specifications. NewCem is a Grade 120 slag cement that meets ASTM C-989 and ASHTO M-302 specifications.

The Grinding Plant has the capacity to grind over 500,000 metric tons of granulated slag. Sales of NewCem in 2002 were 120,000 metric tons and for 2003 were approximately 200,000 metric tons. NewCem product produced by the Lafarge Grinding Plant is distributed through a marine transportation system using the Great Lakes and major rivers through Lafarge distribution terminals located in Red Rock, Minnesota, Kansas City, Missouri and Cleveland, Ohio.

The slag cement manufacturing operations are continually monitored to ensure efficient operation of the Grinding Plant. There are currently sixteen (16) full-time employees at the Grinding Plant; fifteen salaried plant employees and one salaried distribution employee. The annual payroll is approximately \$850,000. Annual tax payments made to the State of Illinois and Cook County are approximately \$326,000. Through its payroll and tax payments, Lafarge supports the depressed economy in the Lake Calumet area and has an active community relations presence through its involvement with the Calumet Area Industrial Commission, Hegewisch Chamber of Commerce, East Side Chamber of Commerce and the Illinois Manufacturers Association.

NewCem is produced at the Lafarge Grinding Plant with state-of-the-art manufacturing technology ensuring consistent supply for customers, exacting quality control to guarantee excellent product quality and minimal environmental impact. The environmental benefits associated with production of NewCem slag cement include productive use of an industrial byproduct, reduced use of virgin materials and reduced energy consumption.

Lafarge's proposal to utilize off-specification used oil fuel in the drying process provides additional environmental benefits by recycling used oils that are continuously generated from

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motor vehicles, refineries and manufacturing operations using machining/cutting oils, heat transfer fluids, hydraulic fluids and general lubricants. Burning used oil is an accepted and proven means of energy recovery in Illinois and throughout the United States. Utilizing off-specification used oil fuel would permit Lafarge to better manage its fuel costs to stay competitive in the market. It would provide additional security for operations at the Grinding Plant and reduce the Company's exposure to the volatility of price and supply of natural gas, a non-renewable source of energy.

- e) **A description of the efforts that would be necessary if the petitioner was to comply with the regulation of general applicability. All compliance alternatives, with the corresponding costs for each alternative, must be discussed. The discussion of costs must include the overall capital costs as well as the annualized capital and operating costs;**

**Response:** Through this Adjusted Standard proceeding, Petitioner seeks a determination by the Board that the slag dryer operated at its South Chicago Plant may be considered a "boiler" for purposes of using off-specification used oil as supplemental fuel. The slag dryer functions as a direct-fired process heater to reduce the moisture content of blast furnace slag so that the slag can be ground into a fine powder and processed into slag cement. The finished slag cement product is used as an architectural building material and in a number of construction and building applications.

In January 2004, the Petitioner requested confirmation from the Illinois Environmental Protection Agency ("IEPA") that the slag dryer could be considered a "boiler" as that term is defined at 35 Ill. Adm. Code 720.110, and was therefore authorized to burn off-specification used oil for energy recovery. By letter dated May 28, 2004, the IEPA through Ms. Joyce L. Munie, P.E., Manager-Permit Section, Bureau of Land, stated that the slag dryer ". . . would not meet the definition of industrial boiler in 35 Ill. Adm. Code 720.110."

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Although Petitioner disagrees with the IEPA's decision and believes that the slag dryer meets the definition of "boiler" in 35 Ill. Adm. Code §720.110, Petitioner would not risk an enforcement action by proceeding to utilize off-specification used oil as a fuel in the slag dryer. As a result of IEPA's interpretation of Section 720.110, Petitioner is prohibited from burning off-specification used oil for energy recovery in its slag dryer. There are no compliance alternatives, no capital improvements and no operational changes that would allow Petitioner to "comply with the regulation of general applicability."

- f) **A narrative description of the proposed adjusted standard as well as proposed language for a Board order that would impose the standard. Efforts necessary to achieve this proposed standard and the corresponding costs must also be presented;**

**Response:** Pursuant to the criteria set forth at 35 Ill. Adm. Code §720.132, the Board may grant the requested Adjusted Standard through a determination that the slag dryer is a boiler, even though it may not otherwise meet the definition of the term "boiler" set forth at 35 Ill. Adm. Code §720.110. Once the Board determines that the Petitioner's slag dryer meets the criteria set forth at 35 Ill. Adm. Code §720.132, it will meet the regulatory definition of the term "boiler" at 35 Ill. Adm. Code 720.110, which states in relevant part:

*Boiler by designation. The unit is one that the Board has determined, on a case-by-case basis, to be a boiler, after considering the standards in Section 720.132.*

An industrial boiler located on the site of a facility engaged in a manufacturing process is authorized under Subpart G of 35 Ill. Adm. Code Part 739 to utilize off-specification used oil for energy recovery. Upon determination by the Board that Petitioner's slag dryer should be classified as a "boiler," it will be allowed to burn off-specification used oil for energy recovery because it will be considered a "Boiler by designation."

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Set forth below is proposed language for a Board Order that would approve the requested Adjusted Standard relief:

1. *Procedural History*
2. *Background*
3. *Agency Recommendation*
4. *Response to Recommendation*
5. *Discussion*
  - *Legal Framework*
  - *Availability of Relief Under Section 720.132*
  - *Section 720.132 Factors*
  - *Other Relevant Factors*
6. *Conclusion*

*The Board finds that Lafarge Midwest, Inc. has established under Section 720.132 of the Board regulations (35 Ill. Adm. Code 720.132), that the slag dryer operated at the South Chicago facility satisfies the criteria set forth in Section 720.132 to be considered a “boiler.” Accordingly, the Board finds and determines that the slag dryer is a “boiler” within the meaning of 35 Ill. Adm. Code 720.110.*

*The Board’s determination that the slag dryer is a “boiler” will allow it to be used for the combustion of off-specification used oil for energy recovery, in compliance with Section 739.161 of the Board’s regulations (35 Ill. Adm. Code 739.161). The Board emphasizes that use of off-specification used oil as fuel for the slag dryer must comply with all other applicable Illinois and federal environmental standards and requirements, including the terms and conditions of Lifetime Operating Permit No. 98010053, issued for operation of the Granulated*

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*Blast Furnace Slag Grinding and Drying Operation and associated air pollution control equipment and any subsequent modifications thereto.*

*This opinion constitutes the Board's findings of fact and conclusions of law.*

**ORDER**

1. *The Board finds that the slag dryer operated by Lafarge Midwest, Inc. at its South Chicago Cement Distribution Terminal/Slag Processing Facility meets the criteria set forth in 35 Ill. Adm. Code §720.132 to be considered a "boiler." The Board accordingly grants Lafarge Midwest, Inc. an Adjusted Standard under 35 Ill. Adm. Code 720.132 and determines that the slag dryer is a "Boiler by designation" under 35 Ill. Adm. Code §720.110.*
2. *The Adjusted Standard will allow the slag dryer to combust off-specification used oil for energy recovery under 35 Ill. Adm. Code 739.161, subject to compliance with all other applicable Illinois and federal environmental standards and requirements.*

*IT IS SO ORDERED.*

- g) **The quantitative and qualitative description of the impact of the petitioner's activity on the environment if the petitioner were to comply with the regulation of general applicability as compared to the quantitative and qualitative impact on the environment if the petitioner were to comply only with the proposed adjusted standard. To the extent applicable, cross-media impacts must be discussed. Also, the petitioner must compare the qualitative and quantitative nature of emissions, discharges or releases that would be expected from compliance with the regulation of general applicability as opposed to that which would be expected from compliance with the proposed adjusted standard;**

**Response:** As noted above, IEPA questioned whether the slag dryer and drying system at the Lafarge Grinding Plant met the definition of a "boiler" in 35 Ill. Adm. Code 720.110. Although Lafarge believes that the slag dryer meets the boiler definition and therefore is allowed to combust off-specification used oil fuels, it is not utilizing off-specification used oil as a fuel in

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the slag dryer. As a result, Lafarge is not able to secure the benefits of used oil recycling and the recovery of thermal energy contained in these materials.

Lafarge will continue to combust substantial quantities of natural gas and suffer the economic uncertainties associated with the volatility of natural gas supplies and costs. As the cost of natural gas increases and availability decreases, the economic success and viability of the slag cement production operation at the Grinding Plant becomes questionable; a production process that utilizes secondary materials from the steel industry that otherwise must be landfilled or otherwise disposed of.

If the Board grants the requested adjusted standard relief, Lafarge would purchase used oil fuel from regulated used oil marketers at a cost per Btu of thermal energy that is significantly less than the escalating cost of natural gas. The used oil fuels would be subject to strict specifications to ensure high Btu value, allow complete combustion and produce negligible change in the combustion exhaust gas composition.

The only consequence associated with the Board's approval of Lafarge's request to utilize used oil fuels in its slag drying system would be a change in the air pollutant emissions from the slag dryer. Currently, the drying system utilizes natural gas as the primary dryer fuel and air contaminants from the combustion process are authorized under Lifetime Operating Permit No. 98010053 issued by IEPA on June 25, 2004. The Operating Permit establishes emissions limitations for particulate matter ("PM/PM<sub>10</sub>"), sulfur dioxide ("SO<sub>2</sub>"), carbon monoxide ("CO"), volatile organic material ("VOM"), and nitrogen oxides ("NO<sub>x</sub>"). Compliance with the permitted emissions limits is achieved by full and complete combustion of the fuel and operation of a high-efficiency fabric filter baghouse system to control emissions in the dryer exhaust.

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Lafarge has investigated how combustion of off-specification used oil fuel would affect air pollutant emissions from the Grinding Plant drying system. Based on representative used oil fuels that would be supplied by reputable, authorized used oil marketers, Lafarge estimates there will be no increases in any of the permitted emissions other than a slight increase in the emissions of sulfur dioxide (SO<sub>2</sub>), as compared to current emissions from combustion of natural gas. Utilization of off-specification used oil fuel in the slag drying system would need to be reviewed and approved by the IEPA air permitting officials, with issuance of a Construction Permit and/or modifications to the existing Operating Permit. Any questions about the air pollutant emissions associated with combustion of used oil fuel would be addressed and fully answered through the air permitting review process.

**h) A statement which explains how the petitioner seeks to justify, pursuant to the applicable level of justification, the proposed adjusted standard;**

**Response:** Section 720.132 of the Board's regulations (35 Ill. Adm. Code §720.132), establishes the criteria to be considered by the Board in making a "case-by-case" determination that certain enclosed devices using controlled flame combustion are boilers, even though they do not otherwise meet the definition of a "boiler" contained in Section 720.110. The criteria for "case-by-case" boiler determination track closely the regulatory definition of "boiler" set forth at 35 Ill. Admin. Code 720.110. Consequently, when evaluating whether a particular combustion source, such as the slag dryer at the Lafarge Drying Plant, should be classified as a boiler, the regulatory definition of "boiler" provides the determining physical characteristics.

Set forth below is the regulatory definition of a "boiler" which identifies the key physical characteristics of a boiler to be considered in making a "case-by-case" boiler determination under 35 Ill. Admin. Code 720.132. The 35 Ill. Admin. Code 720.110 "boiler" definition states:

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**“Boiler”** means an enclosed device using controlled flame combustion and having the following characteristics:

Boiler physical characteristics.

The unit must have physical provisions for recovering and exporting thermal energy in the form of steam, heated fluids, or heated gases; and the unit’s combustion chamber and primary energy recovery sections must be of integral design. To be of integral design, the combustion chamber and the primary energy recovery sections (such as waterwalls and superheaters) must be physically formed into one manufactured or assembled unit. A unit in which the combustion chamber and the primary energy recovery sections are joined only by ducts or connections carrying flue gas is not integrally designed; however, secondary energy recovery equipment (such as economizers or air preheaters) need not be physically formed into the same unit as the combustion chamber and the primary energy recovery section. The following units are not precluded from being boilers solely because they are not of integral design: process heaters (units that transfer energy directly to a process stream) and fluidized bed combustion units; and

While in operation, the unit must maintain a thermal energy recovery efficiency of at least 60 percent, calculated in terms of the recovered energy compared with the thermal value of the fuel; and

The unit must export and utilize at least 75 percent of the recovered energy, calculated on an annual basis. In this calculation, no credit may be given for recovered heat used internally in the same unit. (Examples of internal use are the preheating of fuel or combustion air, and the driving of induced or forced draft fans or feedwater pumps); or

Boiler by designation. The unit is one that the Board has determined, on a case-by-case basis, to be a boiler, after considering the standards in Section 720.132.

**The 35 Ill. Admin. Code 720.132(a) Criteria.** Set forth below is a demonstration that Petitioner’s slag dryer satisfies each of the criteria specified at 35 Ill. Admin. Code 720.132(a) to be considered a boiler.

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***Section 720.132(a) The extent to which the unit has provisions for recovering and exporting thermal energy in the form of steam, heated fluids or heated gases:***

The process unit is a thermal dryer with its main objective being to recover the thermal energy in the fuel being burned in order to heat the slag and drive off moisture. The dryer functions as a direct-fired process heater, in which the process material, wet blast furnace slag, and additional air are brought into contact with the hot combustion product gases. The thermal energy released by the combustion of the fuel is transferred to the wet slag. Heating the slag vaporizes a portion of the moisture that is in the pores of the material. The heat is then exported in the form of heated slag, gases and water vapor. The slag, hot gases and water vapor are discharged from the dryer through a cyclonic separator, where the slag is removed from the exhaust gas stream, which is cleaned by a high-efficiency fabric filter baghouse system before being discharged to the atmosphere. The dried slag captured in the cyclone separators is conveyed to a mill where it is ground to the desired particle size.

The dryer is fully enclosed with an outer shell of steel. The burning chamber is lined with a high temperature resistant refractory material and the transport shaft is lined with ceramic tile. This design is conducive to recovering as much energy as possible from the fuel.

***Section 720.132(b). The extent to which the combustion chamber and energy recovery equipment are of integral design;***

The dryer is fully enclosed and of integral design. The combustion chamber and vertical shaft were assembled to be one piece of equipment. The dryer is an inline portion of the slag cement manufacturing process, in which the slag is dried, ground and size-classified to produce a salable cement product. For a graphic depiction of the slag dryer, see the engineering drawing attached hereto as Exhibit C.

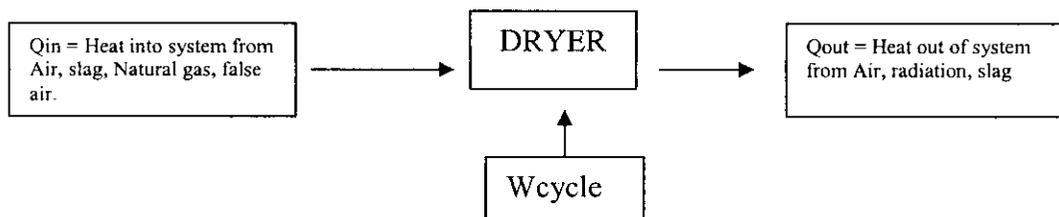
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The regulatory definition of a “boiler” set forth in the Board’s regulations at 35 Ill. Adm. Code 720.110 includes an express exemption from the “integral design” element for process heaters such as the slag dryer. The regulation states, *“The following units are not precluded from being boilers solely because they are not of integral design: process heaters (units that transfer energy directly to a process stream) and fluidized bed combustion units.”*

Because the slag dryer is a direct-fired process heater where the thermal energy of the combusted fuel is transferred to the wet slag being processed, the element of “integral design” is not determinative in this proceeding. However, the slag dryer is fully enclosed and of integral design so compliance with this criterion is established even though the unit is subject to the process heater exemption.

***Section 720.132(c) The efficiency of energy recovery, calculated in terms of the recovered energy compared with the thermal value of the fuel;***

For purposes of calculating the efficiency of energy recovery, a detailed analysis of the South Chicago Drying System is necessary. The South Chicago Drying System can be graphically depicted and summarized with the following process flow diagram:



“Qin” = heat into the system

“Qout” = Energy out of the system

“Wcycle” = net amount of energy transfer by heat and work.

Systems undergoing the drying process as described above deliver a network transfer of energy to the surroundings. This is called a “power cycle”. Thermal efficiency is calculated in engineering thermodynamic reference materials as the following:

$$\eta = W_{cycle}/Q_{in} \text{ eq\#1}$$

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An alternative form based on the balance of the system described above can be:

$$\eta = (Q_{in}-Q_{out})/Q_{in} \text{ eq\#2}$$

Equation #2 translates into: *Efficiency = Energy Absorbed (Q<sub>in</sub>-Q<sub>out</sub>) divided by Q<sub>in</sub> (Heat into system)*

The efficiency method described above is based on the principles of the First and Second Laws of Thermodynamics, hence a method uniformly used worldwide for the design, operation and evaluation of heat systems. (See *Fundamentals of Engineering Thermodynamics*, Michael J. Moran, Third Edition, 1996, pages 60-61; *Chemical and Process Thermodynamics*, B.G. Kyle, Second Edition, 1992, page 63

A heat balance has been calculated for the Slag Drying System to provide the input variables for the thermal efficiency calculations. All values and parameters used in the heat balance calculations are set forth in the following “*Table 1. Heat balance Calculations: Total Heat In*” and “*Table 2. Heat Balance Calculations: Total Heat Out.*”

Table 1. Heat Balance Calculations: Total Heat In

| Line | Feed                 | Definition                 | As Measured (kg/hr) | Moisture Calculation | As measured (dry basis) | Feed   | Kg/Kg_slag | T(C) | CP (kcal/kgC) | Heat (Kcal/Kg Slag) |
|------|----------------------|----------------------------|---------------------|----------------------|-------------------------|--------|------------|------|---------------|---------------------|
| 1    | DF                   | Dilution Fan               | 62,116              |                      | 61,681                  | 61,681 | 0.843      | 22.0 | 0.2421        | 4.4892              |
| 2    | CF                   | Combustion Fan             | 10,800              |                      | 10,724                  | 10,724 | 0.147      | 24.0 | 0.2425        | 0.8531              |
| 3    | FAD                  | Fresh Air Damper           | 17,717              |                      | 17,593                  | 17,593 | 0.240      | 27.0 | 0.2432        | 1.5789              |
| 4    | Slag                 | Slag Feed                  | 81,300              |                      | 73,170                  | 73,170 | 1.000      | 36.0 | 0.1779        | 6.4041              |
| 5    | Slag_H2O             | Slag Water                 |                     | 8,130                |                         | 8,130  | 0.111      | 36.0 | 0.4574        | 1.8296              |
| 6    | DF_H2O               | Dilution Fan Air Water     |                     | 435                  |                         | 435    | 0.006      | 24.5 | 0.4527        | 0.0659              |
| 7    | CF_H2O               | Combustion Fan Air Water   |                     | 76                   |                         | 76     | 0.001      | 27.0 | 0.4537        | 0.0127              |
| 8    | FAD_H2O              | Fresh Air Damper Air Water |                     | 124                  |                         | 124    | 0.002      | 22.3 | 0.4518        | 0.0171              |
| 9    | FUEL_H2O             | Fuel Gas Water             |                     | 42.47                |                         | 42.47  | 0.001      | 25.0 | 0.4529        | 0.0066              |
| 10   | Fuel Latent Heat     |                            | 425                 |                      | 382                     | 382    | 0.005      | 25.0 | 0.2500        | 0.0326              |
| 11   | False Air            |                            | 10,118              |                      | 10,118                  | 10,118 | 0.138      | 23.0 | 0.2423        | 0.7706              |
| 12   | FUEL Combustion Heat |                            | 22,245              |                      | 1,013                   |        |            |      |               | 77.6085             |
| 13   |                      |                            |                     |                      |                         |        |            |      | Total Heat In | 93.6688             |

Outlet

Outlet

Table 2. Heat Balance Calculations: Total Heat Out

|    |  |                 |        |                                      |        |        |       |      |                |         |
|----|--|-----------------|--------|--------------------------------------|--------|--------|-------|------|----------------|---------|
| 14 | False Air in Stack Gas                 |                 | 10,118 | Estimate 10%                         | 10,118 | 10,118 | 0.138 | 72.0 | 0.2536         | 2.5244  |
| 15 | Stack Gas                              |                 | 91,058 |                                      | 90,420 | 90,420 | 1.236 | 72.0 | 0.2536         | 22.5604 |
| 16 | Stack Gas_H2O                          | Stack Gas Water |        | 637                                  | 7,437  | 7,437  | 0.102 | 72.0 | 0.4725         | 3.4582  |
| 17 | Slag                                   | Slag outlet     | 76,500 |                                      | 76,500 | 76,500 | 1.046 | 42.0 | 0.1791         | 7.8642  |
| 18 | Slag H2O                               | Slag water      |        | 1,700                                | 1,700  | 1,700  | 0.023 | 42.0 | 0.4599         | 0.4487  |
| 19 | Radiation                              |                 |        | Approximately 2.5% of total heat out |        |        |       |      |                | 2.2294  |
| 20 | Heat of vaporization                   |                 |        |                                      |        | 6,800  | 0.093 |      | 539            | 50.0916 |
| 21 |  |                 |        |                                      |        |        |       |      | Heat Out       | 89.1769 |
| 22 | Other heat contained within the system |                 |        |                                      |        |        |       |      |                | 4.4920  |
| 23 |  |                 |        |                                      |        |        |       |      | Total Heat Out | 93.6688 |
| 24 |  |                 |        |                                      |        |        |       |      | % Recovery     | 81.04   |

Notes: Slag feed is 85000 kg/hr @10% moisture.

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The following parameters were used to calculate the heat balance for the Slag Drying System:

### Inlet Parameters

$$\text{Heat input from dilution fan (DF)} = (\text{Dry Dilution Fan Airflow (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of Air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of Air @ stream T}$$

$$\text{Heat input from combustion fan (CF)} = (\text{Dry combustion Fan Airflow (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of Air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of Air @ stream T}$$

$$\text{Heat input from Fresh Air Damper (FAD)} = (\text{Dry Fresh Air Damper Airflow (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of Air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of Air @ stream T}$$

$$\text{Heat input from Slag stream} = (\text{Dry Slag Feed Rate (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature Slag Feed before dryer (}^{\circ}\text{C)} * \text{Specific Heat capacity of Slag @ stream T} \text{ ** The slag feed rate was used as the reference material (Kcal/Kg slag)}$$

$$\text{Heat input from water in slag} = (\text{Water mass flow in slag (kg/hour)} * / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature water in slag (}^{\circ}\text{C)} * \text{Specific Heat capacity of water @ stream T}$$

$$\text{Heat input from water in dilution fan air stream} = (\text{Water mass flow in dilution air stream from relative humidity (kg/hour)} * / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of water in dilution air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of water @ stream T}$$

$$\text{Heat input from water in combustion fan air stream} = (\text{Water mass flow in combustion fan air stream from relative humidity (kg/hour)} * / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of water in combustion fan air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of water @ stream T}$$

$$\text{Heat input from water in fresh air damper air stream} = (\text{Water mass flow in fresh air damper air stream from relative humidity (kg/hour)} * / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of water in fresh air damper air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of water @ stream T}$$

$$\text{Heat input from water in Natural Gas stream} = (\text{Water mass flow in gas from moisture provided by gas company (kg/hour)} * / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of water in gas stream from gas company (}^{\circ}\text{C)} * \text{Specific Heat capacity of water @ stream T}$$

$$\text{Heat input from latent heat of natural gas} = (\text{Dry natural gas flow rate (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of natural gas stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of natural gas @ stream T}$$

$$\text{Heat input from false air} = (\text{Dry false air Airflow (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of Air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of Air @ stream T} \text{ *** False air is the air as a result of in-leakage in the system. It is estimated to be about 10% of the stack's air flow rate}$$

$$\text{Heat input from natural gas stream} = \text{natural gas flow rate from gas meter (ft}^3\text{/hour)} * \text{Gas fuel value from gas company (BTU/ft}^3\text{)} * \text{conversion factor to Kcal} / \text{Dry Slag Feed Rate (Kg/hour)}$$

$$\text{Total heat in} = \text{SUM Lines (1 to 12)}$$

### Outlet Parameters

$$\text{Heat output from false air} = (\text{Dry false air Airflow (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of Air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of Air @ stream T} \text{ *** False air is the air as a result of in-leakage in the system. It is estimated to be about 10% of the stack's air flow rate}$$

$$\text{Heat output from stack stream} = (\text{Dry stack stream Airflow (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of Air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of Air @ stream T}$$

$$\text{Heat output from water in stack air stream} = (\text{Water mass flow in stack air stream from relative humidity (kg/hour)} * / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature of water in stack air stream (}^{\circ}\text{C)} * \text{Specific Heat capacity of water @ stream T}$$

$$\text{Heat output from Slag stream} = (\text{Slag mass flow rate after dryer (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature Slag after dryer (}^{\circ}\text{C)} * \text{Specific Heat capacity of Slag @ stream T}$$

$$\text{Heat output from water in slag stream after dryer} = (\text{Water mass flow in slag steam (kg/hour)} / \text{Dry Slag Feed Rate (Kg/hour)}) * \text{Temperature water in slag (}^{\circ}\text{C)} * \text{Specific Heat capacity of water @ stream T}$$

$$\text{Heat output from heat loss thru the system walls} = \text{Total heat out (SUM lines 14 to 18 and line 20)} * 0.025$$

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*Heat output released from the vaporization of water = Water mass flow rate (kg/hr) / Dry Slag Feed Rate (Kg/hour) \* heat of vaporization of water*

*Heat out = (SUM Lines (14 to 18) and Line 20) / 0.975 (stack factor)*

*Other heat contained within the system = Line 13 - Line 21 \*\* This heat includes the radiation heat loss*

*Total heat Out = SUM Lines (21 to 22)*

### **Other Definitions**

- CP = Specific Heat Capacity. At a given temperature, this is the heat input expected from each of the components named above.
- As measure sample: On actual conditions, without moisture adjustments
- Moisture calculation: In the case of the air, the relative humidity and temperature is used along with a Psychrometric chart to determine the Kg of water/Kg of air ratios.
- As measured (Dry basis): Stream of water or material with the moisture removed
- Kg/Kg\_slag : When performing heat balances it is important to select a reference variable. In this case, we selected the slag feed as a reference variable.
- T: The actual temperature of the material or gas stream.
- Heat: The heat consumption can be obtained by multiplying the Kg/Kg\_slag times the temperature times the CP of the individual values.

**False Air Assumption.** Within the cement industry, the accepted industry-wide standard average false air in newer drying systems is estimated to be 10%. This number takes into account devices such as expansion joints, inspection doors/ports, normal equipment wear and any other in-leakage inherent with the system. The assumption is used by reputable design firms and can be verified by any of the well-known equipment manufacturing firm.

Petitioner has verified the wide-spread use of the false air assumption standard through recent consultation with design engineers from F.L. Smidth Group, an international engineering, manufacturing and design firm that specializes in the cement and mineral industries. The principal engineering contact at F. L. Smidth Group was:

Mr. Peter Paone, Process Engineer - Process Design  
F.L. Smidth Group  
2040 Avenue C- Bethlehem, Pennsylvania 18017-2188  
(610) 264 6496

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**Shell Radiation Assumption.** Within the cement industry, the accepted industry-wide standard for average for shell radiation from newer dryers is estimated to be at 2.5%. This estimate refers to the shell losses in the system.

Petitioner verified wide-spread use of the shall radiation assumption standard through recent consultation with design engineers from F.L. Smidth Group, an international engineering, manufacturing and design firm that specializes in the cement and mineral industries. The principal engineering contact at F. L. Smidth Group was:

Mr. Peter Paone, Process Engineer - Process Design  
F.L. Smidth Group  
2040 Avenue C- Bethlehem, Pennsylvania 18017-2188  
(610) 264 6496

**Thermal Energy Recovery Efficiency Calculation.** The definition of the term “boiler” at 35 Ill. Admin. Code 720.110 specifies a standard for thermal energy recovery efficiency for a boiler. The relevant portion of the definition (which is identical to the federal definition) states: “While in operation, the unit must maintain a thermal energy recovery efficiency of at least 60 percent, calculated in terms of the recovered energy compared with the thermal value of the fuel”

Calculations to demonstrate compliance with the 60% thermal energy recovery efficiency standard of Section 721.110 were performed as described below:

- Thermal value of the fuel from line# 12 “Table 1. Heat Balance Calculations: Total Heat In” = **77.6085 Kcal/Kg\_Slag**
- Recovered Energy = Energy used by the system. This value is calculated as follows:
  - o The total value of energy used (based on a one year production period) is calculated by subtracting the total energy consumed in a one year period minus the pre-heat portion of the system (1.5% of the total energy used). The total energy was calculated by multiplying the known energy consumption from the heat balance (93.6688 Kcal/Kg\_Slag) with the total Kg of slag used in 2002

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(111,991,000). To this number, subtract the 1.5% of energy used in the pre-heating process of the furnace.

- o In order to calculate the recovered energy (energy absorbed) from the system, to the total heat value calculated above, we will subtract all heats that leave the system (False air in stack gas, stack gas, stack gas H<sub>2</sub>O, and Radiation)
- o The value obtained from the step above is **61.69 Kcal/Kg slag**
- Finding the thermal energy recovery as per 40 CFR 260.10(1)(iii): The last step is to divide the recovered energy (energy absorbed) by the Thermal value of the fuel:  **$61.69/77.61 * 100 = 79.23\%$**

As demonstrated by the foregoing calculations (and supported by the heat balance calculations), the Slag Drying System achieves a thermal energy recovery efficiency of 79.23%. The thermal energy recovery efficiency clearly exceeds the Section 720.110 criteria of a minimum of 60% recovery.

***Section 720.132(d) The extent to which exported energy is utilized;***

The definition of the term “boiler” at 35 Ill. Admin. Code 720.110 specifies a standard for utilization of the recovered thermal energy for a boiler. The relevant portion of the definition (which is identical to the federal definition) states: “The unit must export and utilize at least 75 percent of the recovered energy, calculated on an annual basis. In this calculation, no credit may be given for recovered heat used internally in the same unit. (Examples of internal use are the preheating of fuel or combustion air, and the driving of induced or forced draft fans or feedwater pumps.)”

Internal use of the recovered heat only occurs during preheating every time the system is started. The preheating hours account for 1.5% of the total operating hours in a year. With the loss of 1.5 percent of the fuel heat input due to preheating the dryer, the annual energy recovery is estimated to be 79.23%.

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| Total Kcal used without heat of drying | Total Kg of slag from 2002 | Kcal/hg slag | % Used in Pre-Heat | Kcal/kg slag used in pre-heat | %Recovery after subtracting preheat used |
|--|----------------------------|--------------|--------------------|-------------------------------|--|
|  | 111,991,000                | 93.67        | 1.50%              | 157,350,997                   |  |
| 10,332,715,500                         |                            | 92.26        |                    |                               | 79.23%                                   |

***Section 720.132(e) The extent to which the device is in common and customary use as a “boiler” functioning primarily to produce steam, heated fluids or heated gases.***

Direct-fired dryers and process heaters are widely used in the production of cement and other non-metallic mineral products. Cement kilns and the associated process heaters and dryers used in the production of Portland cement utilize a tremendous amount of fuel to dry the raw materials before being introduced into the pyroprocessing steps and to produce the extreme temperatures and long residence times needed to calcine limestone rock, shale, sand and other minerals to produce clinker and ultimately Portland cement. It is a matter of common knowledge that cement kilns utilize a variety of fuel types including coal, petroleum coke, specification and off-specification used oil, used vehicle tires and hazardous wastes in a safe and environmentally sound manner under express authorization and approvals from state and federal environmental regulatory agencies.

Lafarge operates a large Portland cement manufacturing plant located near Alpena, Michigan. The Alpena Plant is Lafarge’s largest Portland cement-producing facility and reputed to be the largest cement manufacturing facility in North America. The plant consists of five cement kilns that produce approximately 2.7 million tons of cement annually. At Alpena, cement is made from high quality limestone, silica, alumina and iron. The limestone is crushed into nuggets, which are transported by conveyor to the plant. There, the limestone and other raw materials are dried in the raw feed dryers and fed into raw grinding mills which grind and blend

the raw feed mixture into a fine powdered kiln feed. This “raw grind” kiln feed is conveyed into rotary cement kilns where it is heated to over 2700<sup>0</sup> Fahrenheit becoming grayish-black nuggets called clinker. When the clinker emerges from the kiln, it is cooled, mixed with gypsum, and ground into the fine powder known as Portland cement.

Lafarge is committed to sustainable development and the Alpena Plant has served as a showcase for several environmentally beneficial recycling projects. For example, the Alpena Plant is one of the few North American cement plants to use waste heat from the cement kilns to generate steam which drives turbines that produce electricity to power the plant’s internal electrical system. Additionally, through a program known as “industrial ecology” Lafarge has implemented projects to utilize the waste byproducts of two other manufacturing processes as raw materials used in the manufacture of Alpena cement. The projects result in a reduction in the total waste stream from the plant while maintaining the high-quality cement for which the plant is known.

Another recycling opportunity implemented by Lafarge at the Alpena Plant was the utilization of off-specification used oil as fuel in the raw grind dryers. The State of Michigan administers a used oil regulatory program that is virtually identical to the federal and Illinois used oil management programs. Consequently, Lafarge consulted with the Michigan Department of Environmental Quality (“DEQ”) to secure approval to combust off-specification used oil fuel in the raw grind dryers. Under the DEQ-administered used oil/RCRA regulations, specifically Michigan DEQ rules R299.9814 and 299.9101, Lafarge was required to demonstrate that the Alpena raw grind dryers satisfied the physical boiler criteria established by USEPA (and adopted by both Illinois and Michigan), to demonstrate use of used oil fuel in the dryer constituted a legitimate use for energy recovery. As noted above, those physical criteria are set

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forth in the definition of “boiler” and rely upon the concepts of integral design, combustion efficiency and energy recovery.

The Michigan DEQ reviewed the design, combustion efficiency and energy recovery attributes of the raw grind dryers and determined that the “boiler” criteria were established for these process heaters. Because the DEQ officials determined that the physical criteria were met, Lafarge was given approval to proceed with the combustion of off-specification used oil fuel in the raw grind dryers. The Michigan DEQ approved the use of used oil fuel by a detailed analysis of the dryer information provided by Lafarge, and did not require Lafarge to seek a variance or adjusted standard through the “boiler by designation” process. A copy of the Michigan DEQ’s April 2, 2004 determination is attached hereto as Exhibit D.

The raw slag dryer utilized at Lafarge’s Grinding Plant is the same type of combustion source as the raw grind dryers at Lafarge’s Alpena cement plant that were authorized by the Michigan DEQ to combust off-specification used oil. With respect to the physical criteria established in the definition of “boiler,” specifically integral design, combustion efficiency and energy recovery, the South Chicago slag dryer and the Alpena raw grind dryers are virtually identical combustion sources. The Michigan DEQ’s determination that the Alpena dryers meet the boiler physical characteristics and therefore are authorized to combust off-specification used oil fuel is an excellent example that such dryers, including the slag dryer at the Grinding Plant, are combustion sources *“in common and customary use as a “boiler” functioning primarily to produce steam, heated fluids or heated gases.”* Moreover, it demonstrates that the Board’s approval to grant the adjusted standard relief requested in this proceeding would be consistent with the findings of other environmental regulatory authorities.

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***Section 720.132(f) Other relevant factors.***

The federal used oil/RCRA regulations at 40 CFR 260.33 specify the procedures for making a case-by-case determination that a particular combustion device, such as the slag dryer operated at Lafarge's Grinding Plant, should be considered a "boiler" for purposes of utilizing off-specification used oil fuels. The federal regulations define the term "boiler" (40 CFR 260.10); allow the combustion of off-specification used oil in boilers (40 CFR 279.61); and specify the criteria to determine which combustion devices can be considered equivalent to a boiler and allowed to combust off-specification used oil (40 CFR 260.32.) As noted above, the Pollution Control Board has completed "identical-in-substance" rulemakings to adopt these federal RCRA regulations as the Illinois regulations applicable to the combustion of off-specification used oil in boilers and similar combustion devices.

In promulgating the referenced RCRA regulations, USEPA has explained the scope of the regulations and discussed application of the rules to specific fact patterns. Those explanations and interpretations are set forth in the preamble discussions that accompany the rulemakings published in the Federal Register. In its legislative capacity, the Board has relied on the USEPA preamble discussion to support its own rulemaking efforts and at times, has actually adopted USEPA guidance as mandatory and not advisory. (See the Board's recent rulemaking in R03-18 and its determination in that rulemaking that USEPA's RCRA guidance for delisting hazardous wastes was mandatory and not solely advisory.)

Consequently, the justifications set forth by USEPA to explain and interpret the criteria for making "case-by-case" boiler determinations can and should be relied upon by the Board in reviewing Lafarge's request for adjusted standard relief. In its November 29, 1985 rulemaking for the used oil management standards (50 *Federal Register* 49164), USEPA explained why it

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was allowing combustion of off-specification of used oil in industrial boilers but not in "...nonindustrial boilers (e.g., located in apartment and office buildings, schools, hospitals.)" USEPA focused on the risks of burning off-specification used oil in such "nonindustrial" combustion sources due to proximity to highly populated areas. According to USEPA, due to a greater number of "nonindustrial" boilers and the location of such sources in populated areas, these combustion sources would potentially expose many more individuals to hazardous emissions from burning off-specification used oil fuels.

Combustion of off-specification of used oil in industrial (and utility) boilers was believed by USEPA as presenting a much lower risk because such boilers are not located in close proximity to populated areas and "...large boilers or industrial furnaces may be operated by trained operators and equipped with combustion controls sophisticated enough to maintain peak combustion efficiency when burning fuels the unit is not designed to burn. Further, many industrial furnaces and some boilers are equipped with particulate control equipment that may adequately control emissions from metal-bearing waste fuels." (50 *Federal Register* 49164 at 49182),

As evidenced by USEPA's preamble discussion, the agency considered four basic criteria in permitting combustion of off-specification used oil in industrial but not "nonindustrial" combustion sources: (1) location away from populated areas; (2) operation by trained operators; (3) maintaining good combustion efficiency to destroy organics; and (4) pollution control equipment to control particulate matter emissions (including metal particulate emissions.) In addition, USEPA has defined certain physical characteristics of boilers to distinguish boilers used to reclaim thermal energy from used oil or waste from other devices designed primarily to dispose of wastes without legitimate thermal recovery.

As set forth above, the design, combustion efficiency and energy recovery attributes of the slag dryer satisfy the physical boiler criteria established by USEPA and the Board. In addition, the non-physical criteria that justify combustion in industrial boilers versus non-industrial boilers or other combustion sources are satisfied in this situation.

First, the Drying Plant is located in a heavily industrialized area of Cook County that is remote from any residential development. The Grinding Plant and the drying system, in particular, is operated by trained personnel. The slag dryer is equipped with of state-of-the-art, efficient combustors and operating controls to maximize complete combustion of the fuels. Good combustion controls are designed into the system to maximize the extraction of all Btu value from the fuels combusted. Since fuel costs are critical to the overall profitability of the Grinding Plant, maximizing fuel efficiency is always a top priority, even if Lafarge is allowed to use lower cost off-specification used oil fuels.

Finally, the slag dryer is equipped with a modern, high-efficiency fabric filter baghouse particulate control system to minimize the release of PM and other air contaminants in the exhaust gases. The combined capture and removal efficiency of these baghouse systems typically achieve greater than 99.9% overall control efficiency. Again, maximizing capture of the dried slag is another component of plant productivity and profitability that is critical to the overall financial health and long-term viability of the facility.

- i) **A statement with supporting reasons that the Board may grant the proposed adjusted standard consistent with federal law. The petitioner must also inform the Board of all procedural requirements applicable to the Board's decision on the petitioner that are imposed by federal law and not required by this Subpart. Relevant regulatory and statutory authorities must be cited;**

**Response:** The Board may grant the adjusted standard relief requested by Lafarge consistent with federal law. Section 7.2 and 22.4(a) of the Illinois Environmental Protection Act

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[415 ILCS 5/7.2 and 22.4(a)] require the Pollution Control Board to adopt regulations that are “identical in substance” to the hazardous waste regulations adopted by the USEPA. The USEPA hazardous waste regulations implement Subtitle C of the federal Resource Conservation and Recovery Act of 1976 [RCRA Subtitle C, 42 U.S.C. 6921, et seq.].

The federal RCRA regulations contain identical provisions for making a determination that a particular combustion device, such as the slag dryer operated at Lafarge’s Grinding Plant, should be considered a “boiler” for purposes of utilizing off-specification used oil fuels. That federal regulation is set forth at 40 CFR 260.32 “*Variance to be classified as a boiler.*” Although the Illinois analog uses the term “adjusted standard” rather than “variance” to describe the agency “case-by-case” boiler determination, the standards, criteria and procedures are identical.

In short, the Illinois hazardous waste management regulations are “identical in substance” to the federal RCRA regulations and both state and federal regulations provide a mechanism to determine “...on a case-by-case basis that certain enclosed devices using controlled flame combustion are boilers, even though they do not otherwise meet the definition of boiler contained in Section 260.10.” The federal regulation is set forth at 40 CFR 260.32 and the “identical in substance” Illinois regulation is set forth at 35 IAC 720.132. Approval by the Board of Lafarge’s Petition would be consistent with federal law and the implementing RCRA regulations.

- j) A statement requesting or waiving a hearing on the petition (pursuant to Section 104.422(a)(4) of this Part a hearing will be held on all petitions for adjusted standards filed pursuant to 35 Ill. Adm. Code 212.126 (CAA));**

**Response:** Petitioner waives its right to a hearing on the Petition.

- k) The petition must cite to supporting documents or legal authorities whenever they are used as a basis for the petitioner’s proof. Relevant portions of the**

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**documents and legal authorities other than Board's decisions, State regulations, statutes and reported cases must be appended to the petition;**

**Response:** Relevant portions of all documents or other information sources that have been used to support this Petition are attached or have been cited in the foregoing text of the Petition.

**l) Any additional information which may be required in the regulation of general applicability.**

**Response:** The regulation of general applicability does not specify any additional information requirements that must be addressed in this Petition. However, Lafarge requests that the Board consider the determinations made by other regulatory authorities to allow the combustion of off-specification used oil in controlled flame combustion devices such as raw material dryers and process heaters. As noted previously, the Michigan DEQ has determined that the raw grind dryer at Lafarge's Alpena cement plant meets the physical characteristics of a "boiler" that are specified in the used oil/RCRA regulations and approved Lafarge's request to utilize off-specification used oil as fuel in the dryer. The slag dryer in use at Lafarge's South Chicago Slag Grinding Plant is virtually identical to the raw grind dryer approved by the Michigan DEQ. The technical and regulatory analysis conducted by Michigan DEQ officials should be considered by the Board in evaluating Lafarge's request to utilize used oil fuel in the slag dryer at its South Chicago Slag Grinding Plant.

WHEREFORE, Petitioner requests a determination from the Illinois Pollution Control Board that the slag dryer operated at the South Chicago Slag Grinding Plant satisfies the criteria

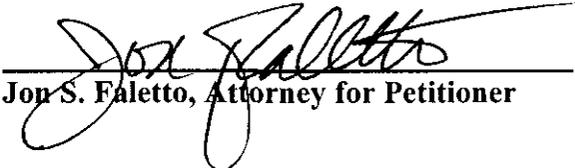
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set forth in Section 720.132; is a “Boiler by designation” within the meaning of 35 Ill. Adm. Code 720.110; and may utilize off-specification used oil for energy recovery, in compliance with Section 739.161 of the Board’s regulations (35 Ill. Adm. Code 739.161).

**Respectfully submitted,**

**LAFARGE MIDWEST, INC., Petitioner**

**By:**

  
\_\_\_\_\_  
**Jon S. Faletto, Attorney for Petitioner**

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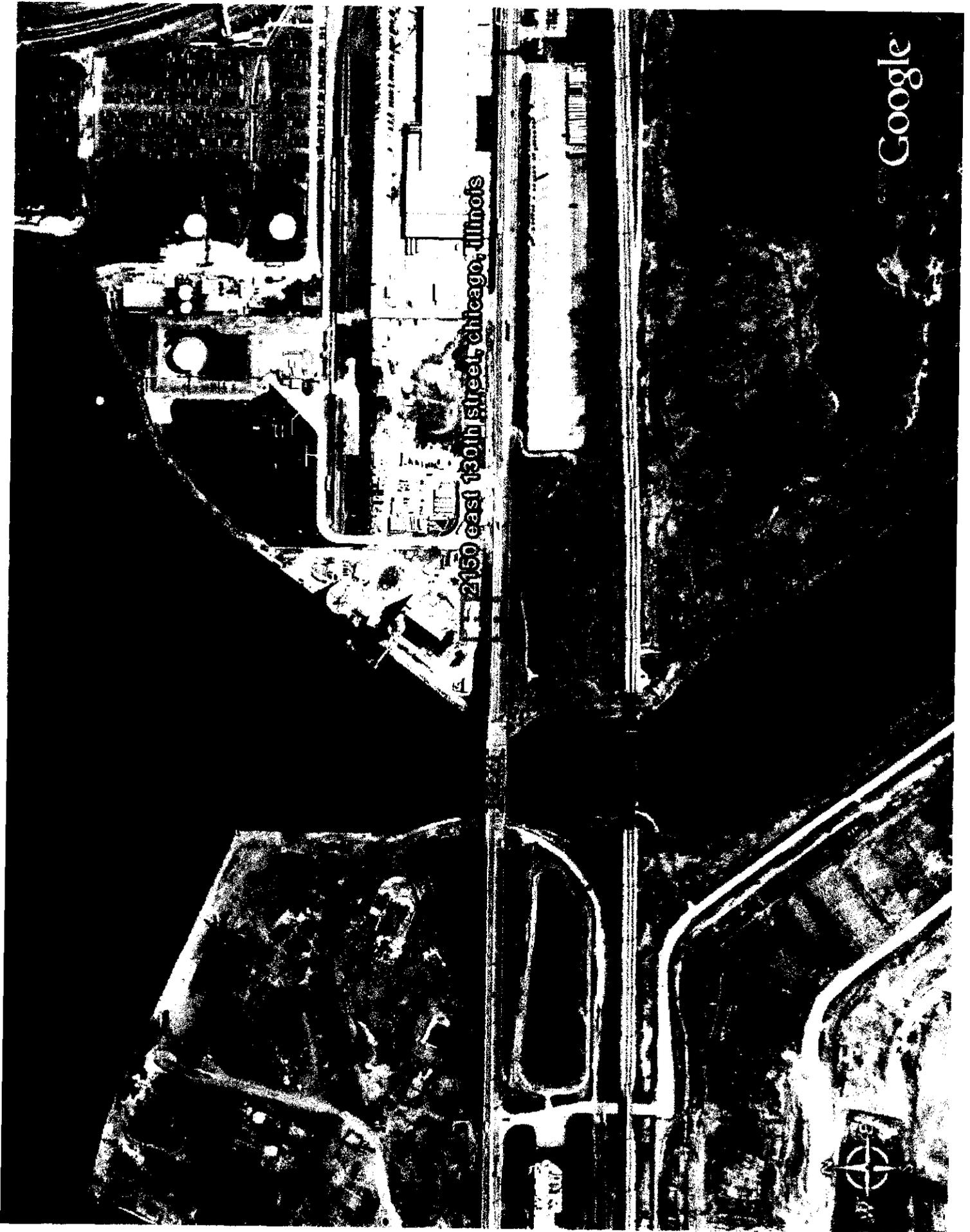
## LIST OF EXHIBITS

- Exhibit A: Aerial Photograph of Grinding Plant**  
(Source: *Google Earth*® Database)
- Exhibit B: Map Depicting Grinding Plant and South Lake Calumet Area**  
(Source: USEPA *Enviromapper* Database)
- Exhibit C: Engineering Drawing of Slag Dryer**
- Exhibit D: Michigan DEQ Correspondence (April 2, 2004) - Approval for Off-Specification Used Oil Fuel in Alpena Raw Grind Dryer**

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# Exhibit A



Google

# Exhibit B



# Exhibit C



# Exhibit D



JENNIFER M. GRANHOLM  
GOVERNOR

STATE OF MICHIGAN  
DEPARTMENT OF ENVIRONMENTAL QUALITY  
LANSING



STEVEN E. CHESTER  
DIRECTOR

April 2, 2004

Mr. Bob Budnik  
Environmental Manager  
Lafarge North America  
Great Lakes Region – Alpena Plant  
P.O. Box 396  
Alpena, Michigan 49707

Dear Mr. Budnik:

Thank you for your February 20, 2004, letter to Mr. G. Vinson Hellwig, Chief, Air Quality Division (AQD), Department of Environmental Quality (DEQ), regarding the proposed use of off-specification used oil fuel in the raw grind dryer. As your letter requests a determination that the dryer is an industrial boiler pursuant to the administrative rules promulgated under Part 111, Hazardous Waste Management, of the Natural Resources and Environmental Protection Act, 1994 PA 451, as amended (NREPA), the DEQ, Waste and Hazardous Materials Division (WHMD), is responding directly to your request.

As you know, off-specification used oil fuel can be burned for energy recovery only in certain types of units defined in R 299.9814(3)(a). One of the specified units is an industrial boiler that is located on the site of a facility that is engaged in a manufacturing process where substances are transformed into new products, including component parts of products, by mechanical or chemical processes. An industrial boiler must also be a boiler as defined in R 299.9101(w).

According to your letter, the raw grind dryer functions as a direct-fired process heater to produce heated gases that act directly upon the raw materials fed to the unit to drive off moisture. The dryer is fully enclosed within an outer shell of steel, and the burning chamber is lined with refractory material and ceramic tile to recover the energy of the fuel. Based upon this explanation, the WHMD agrees that the unit has physical provisions for recovering and exporting thermal energy in the form of heated gases and satisfies this requirement for classification as a boiler.

In order to be considered a boiler, the combustion chamber and primary energy recovery section of the unit shall be of integral design. However, process heaters are not required to meet the integral design criteria for classification as a boiler. The AQD district staff agrees that the raw grind dryer is a process heater and, therefore, is not required to meet this design requirement for classification as a boiler.

There is also an efficiency requirement for classification as a boiler. The information provided in your letter indicates that the raw grind dryer satisfies the efficiency criteria for both energy recovery and exportation of recovered energy.

Based on this analysis, the WHMD concurs that the raw grind dryer is a boiler and, specifically, an industrial boiler for purposes of implementing the used oil management standards of Part 111.

Be aware that the use of off-specification used oil fuel may impact any designations held by the company under Part 115, Solid Waste Management, of the NREPA, as a change in the materials and processes used may affect waste generation. Lafarge must take the actions necessary to maintain the validity of these designations.

If you have any questions regarding this letter, please contact Mr. Jack Schinderle, Hazardous Waste and Radiological Protection Section, WHMD, at 517-373-8410.

Sincerely,



George W. Bruchmann, Chief  
Waste and Hazardous Materials Division  
517-373-9523

cc: Mr. Bob Cooper, Lafarge North America  
Mr. Brian Gasiorowski, Lafarge North America  
Mr. G. Vinson Hellwig, DEQ  
Mr. Phil Roycraft, DEQ  
Mr. Duane Roskoskey, DEQ  
Mr. Jack Schinderle, DEQ  
Mr. Mark Stephens, DEQ